

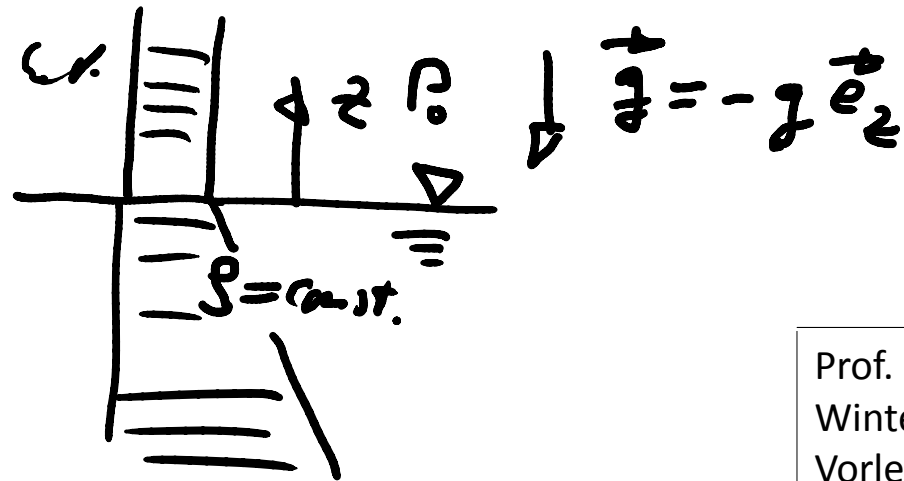
Weitere Spezialisierung

Hydrostatik $\vec{p} \equiv \sigma$, da keine Relativbewegung
zwischen Flüssigkeitsteilchen.

$$\rho \frac{D\vec{u}}{Dt} = \sigma$$

$\vec{p} = -\rho \vec{g}$ Hydrostatische Grundgleichung.

z.B. Druckbestimmung, schwere Flüssigkeit



$$\frac{dP}{dz} \vec{e}_z = -\rho \vec{g}$$

$$P(z) = -\rho g z + P_0$$

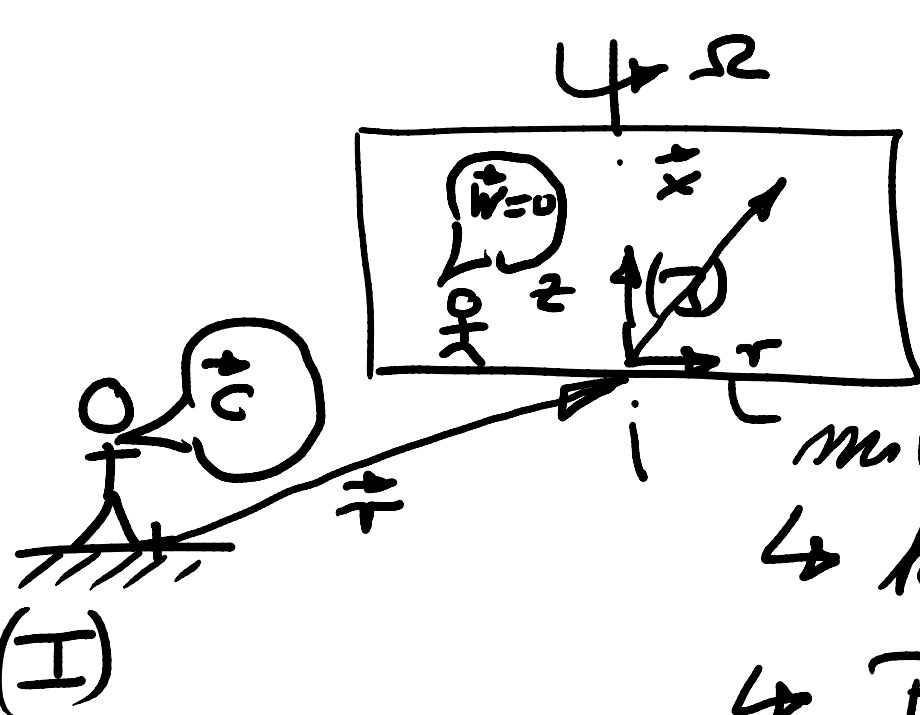


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Fluidsysteme

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Wintersemester 2012/13
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$$\vec{c} = \vec{w} + \vec{u} + \vec{U}$$

$$\vec{U} = \left[\frac{D\vec{x}}{Dt} \right]_I ; \vec{w} = \left[\frac{D\vec{x}}{Dt} \right]_B$$

mit bewegtes System

↳ keine Relativgeschw.

$$\vec{p} \equiv 0$$

$$\rho \frac{D\vec{w}}{Dt} \equiv 0$$

\vec{w} Relativgeschw.

$$\vec{u} \text{ Umfahrgeschw. } \vec{u} = \vec{\Omega} \times \vec{r}$$

\vec{U} Führunggeschw.

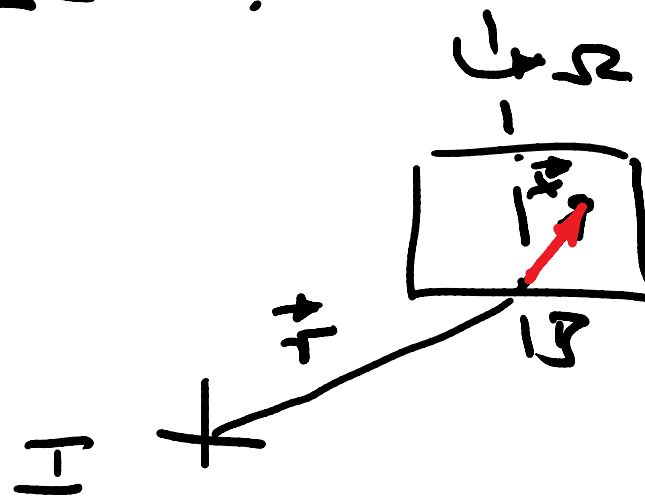
\vec{c} Absolutgeschw.



$$\vec{c} = \left[\frac{D \vec{x}}{Dt} \right]_{\mathcal{B}} + \left[\frac{D \vec{r}}{Dt} \right]_{\mathcal{I}} + \vec{\Omega} \times \vec{r}$$

\mathcal{B} : Beschränktes System

\mathcal{I} : Inertialsystem



$$\vec{c} = \left[\frac{D}{Dt} (\vec{x} + \vec{r}) \right]_{\mathcal{I}} = \left[\frac{D \vec{x}}{Dt} \right]_{\mathcal{I}} + \left[\frac{D \vec{r}}{Dt} \right]_{\mathcal{I}}$$

$$\left[\frac{D \vec{x}}{Dt} \right]_{\mathcal{I}} = \left[\frac{D \vec{x}}{Dt} \right]_{\mathcal{B}} + \vec{\Omega} \times \vec{x}$$

gilt allgemein für eine beliebige Vektor \vec{b} z.B.

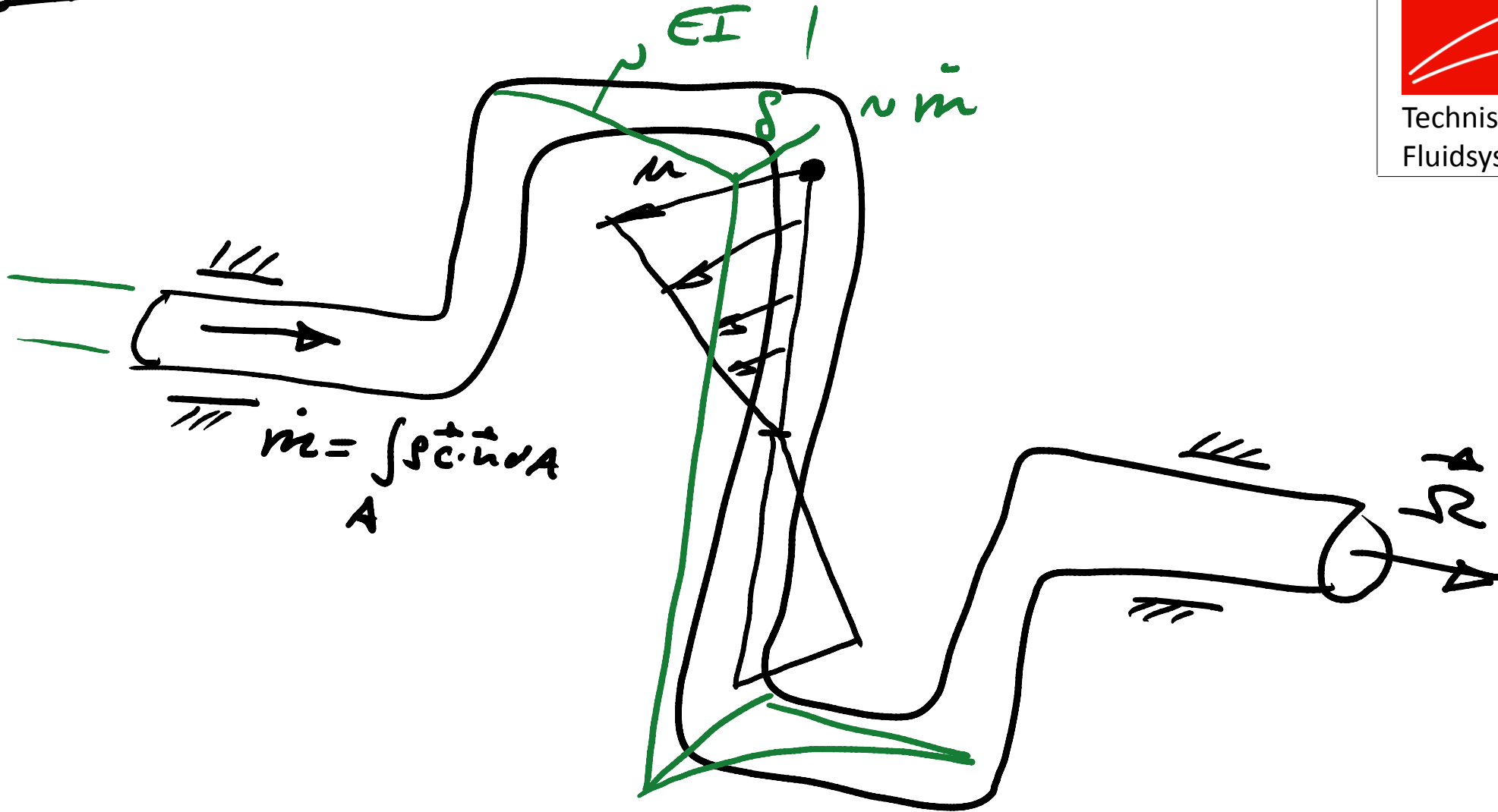
$$\vec{I} = \int \rho \vec{c} \, dV$$

$$\vec{\Omega} = \int \rho \vec{x} \times \vec{c} \, dV$$

$$\left[\frac{D \vec{b}}{Dt} \right]_{\vec{I}} = \left[\frac{D \vec{b}}{Dt} \right]_{\vec{II}} + \vec{\Omega} \times \vec{b} + \dots$$



Beispiel Controlvolumen

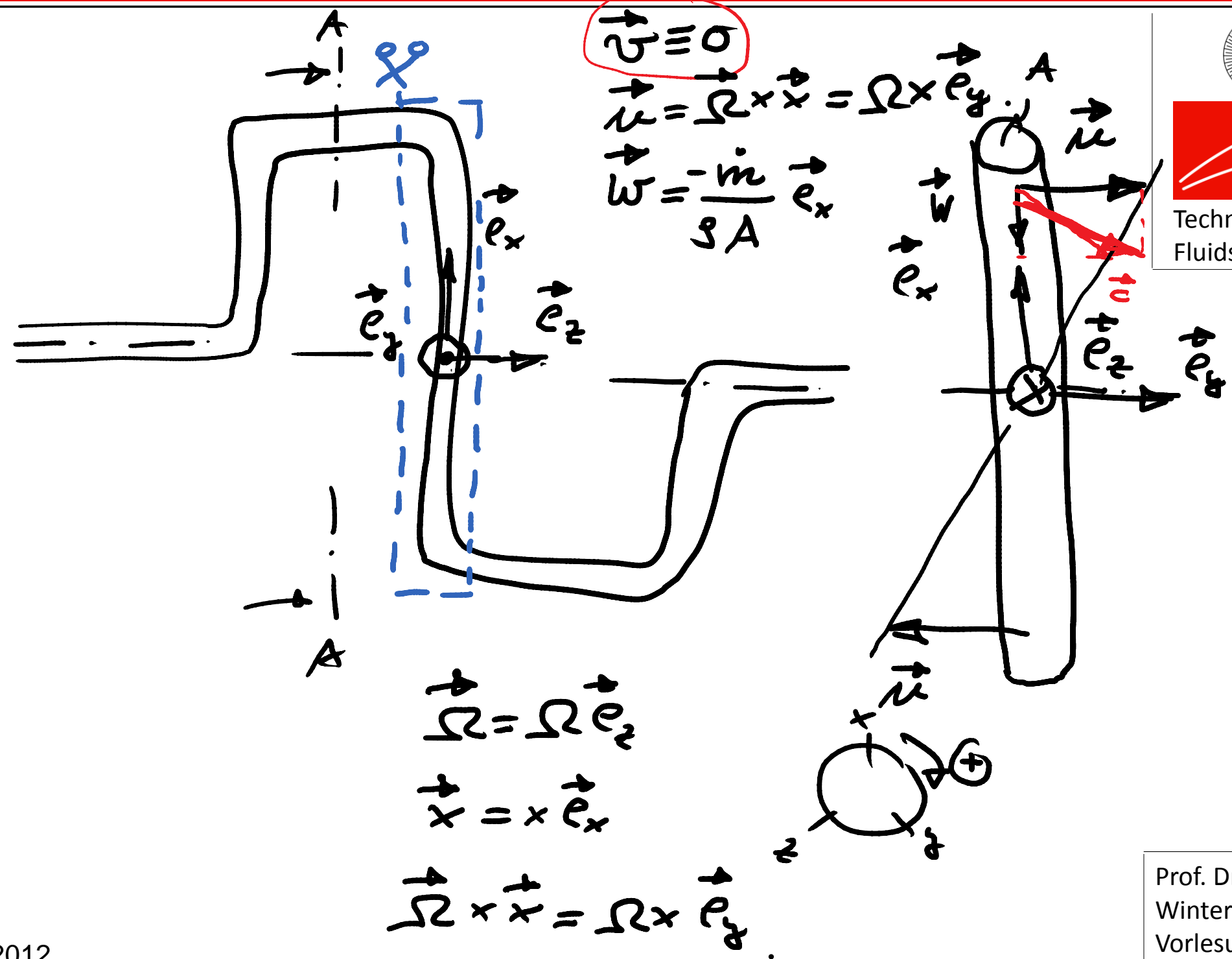


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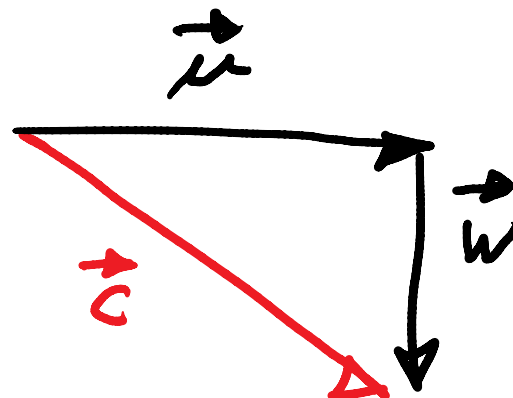
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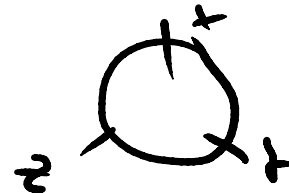


$$\left[\frac{D\vec{I}}{Dt} \right]_I = \vec{F}$$

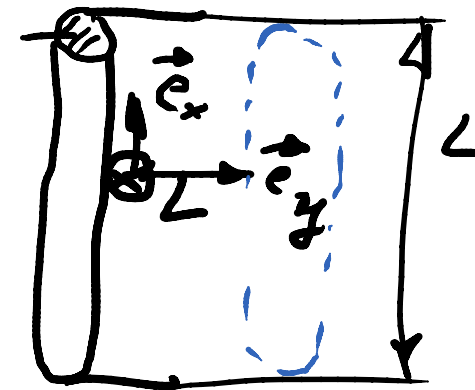


Geschwindigkeitssdreieck.

$$\vec{I} = \int_V \rho \vec{c} dV = \int_V \rho (\vec{u} + \vec{w}) dV$$



$$\left[\frac{D\vec{I}}{Dt} \right]_I = \underbrace{\left[\frac{D\vec{I}}{Dt} \right]_I}_{\equiv 0} + \underbrace{\vec{\Omega} \times \vec{I}}_{\text{Coriolis}} = \vec{F} = \Omega m L \vec{e}_2 \times \vec{e}_x = -\Omega m L \vec{e}_y \quad m = \rho V = \rho w s A$$



$$= \underbrace{\vec{\Omega} \times \int_V \rho (\vec{\Omega} \times \vec{x}) dV}_{\equiv 0} + \underbrace{\vec{\Omega} \times \int_V \rho \vec{w} dV}_{\text{Coriolis}} = \vec{\Omega} \times \rho \vec{w} A L$$



$$\rho \left[\frac{D\vec{c}}{Dt} \right]_I = \nabla \cdot \vec{T} + \vec{f}$$

$$\rho \left[\frac{D\vec{c}}{Dt} \right]_B + \rho \vec{\Omega} \times \vec{c} = \nabla \cdot \vec{T} + \vec{f}$$

$$\vec{c} = \vec{w} + \vec{u} + \vec{\Omega} \times \vec{x}$$

Scheinkräfte

$$\rho \left[\frac{D\vec{w}}{Dt} \right]_B = \nabla \cdot \vec{T} + \vec{f} - \rho \left(\vec{a} + 2 \vec{\Omega} \times \vec{w} + \left(\vec{\Omega} \times (\vec{\Omega} \times \vec{x}) \right) + \rho \vec{\Omega} \times \dot{\vec{x}} \right)$$



$$\vec{\nabla} p = \vec{\rho} \vec{g}$$

Hydrostatische
Gleichg.

$$\vec{\rho} \vec{g} = -\vec{\nabla} \psi^*$$

ψ^* ist das Potential
des Volumenkrafts.

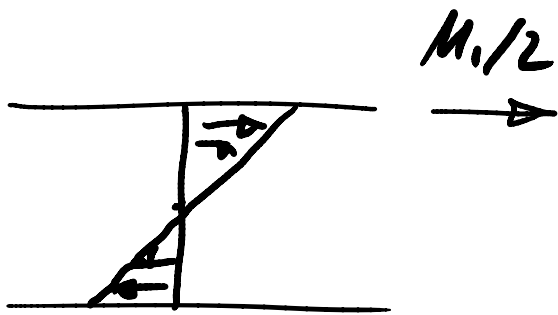
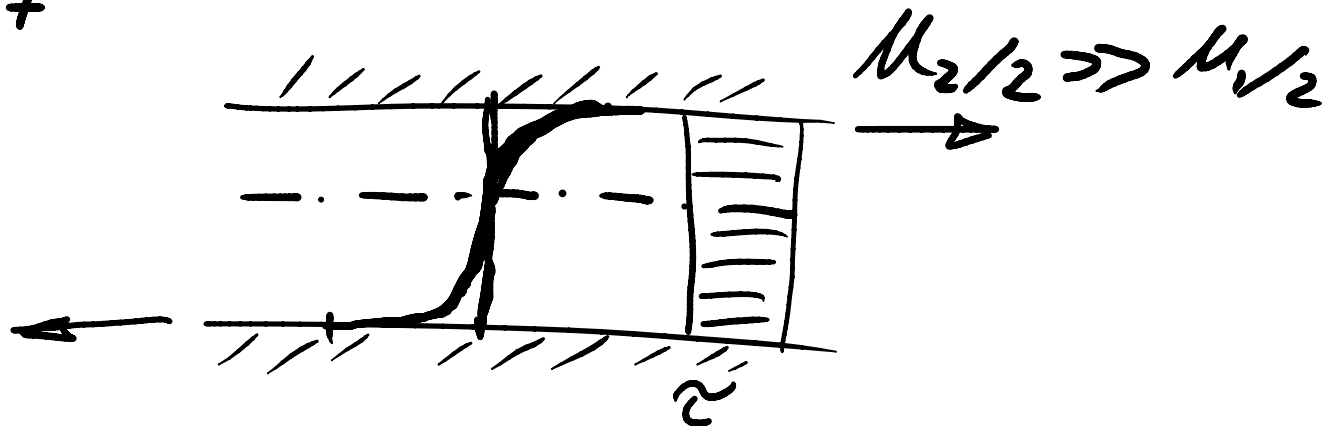
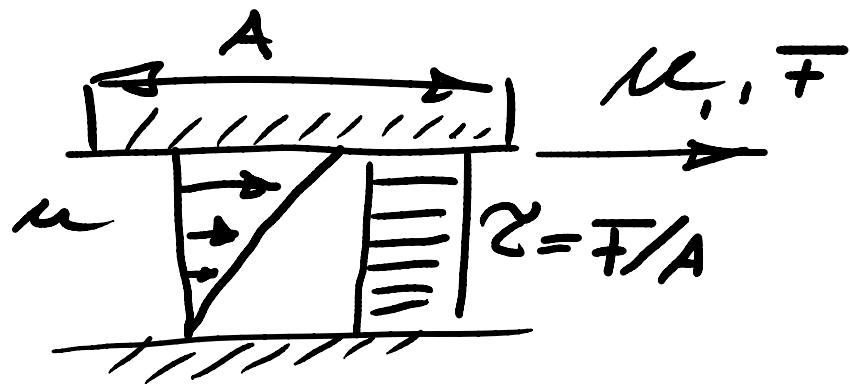
z.B.

$$\psi^* = \rho g z + \text{const.} \quad \text{Potential des Schw.$$

$$\psi^* = \frac{1}{2} \rho \Omega^2 r^2 + \text{const.} \quad \text{Potential des Zentrifugalkrafts.}$$

$$\underline{\underline{\rho + \psi^* = \text{const}}}$$

Geschwindigkeitsverteilung im Spalt
 infolge schlepp Vönd und infolge
 Druckverdr.



$-u_1/2$ laminare Couette str.

turbulente Couette str.



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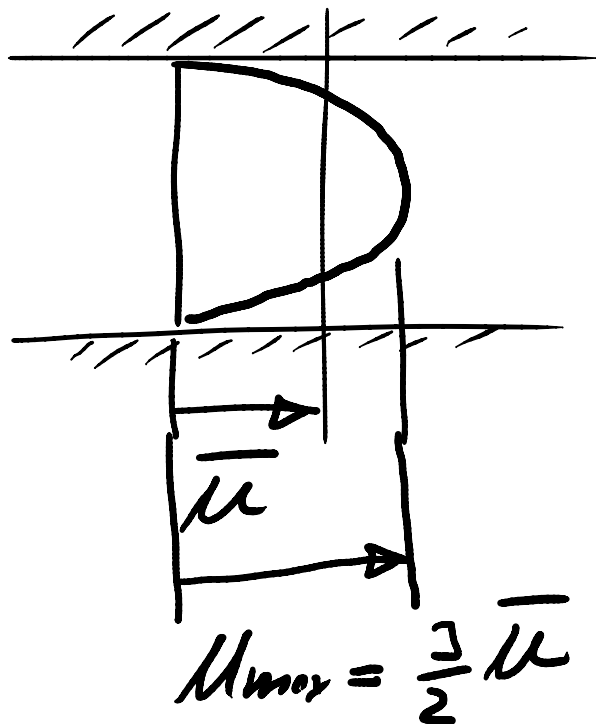


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2D

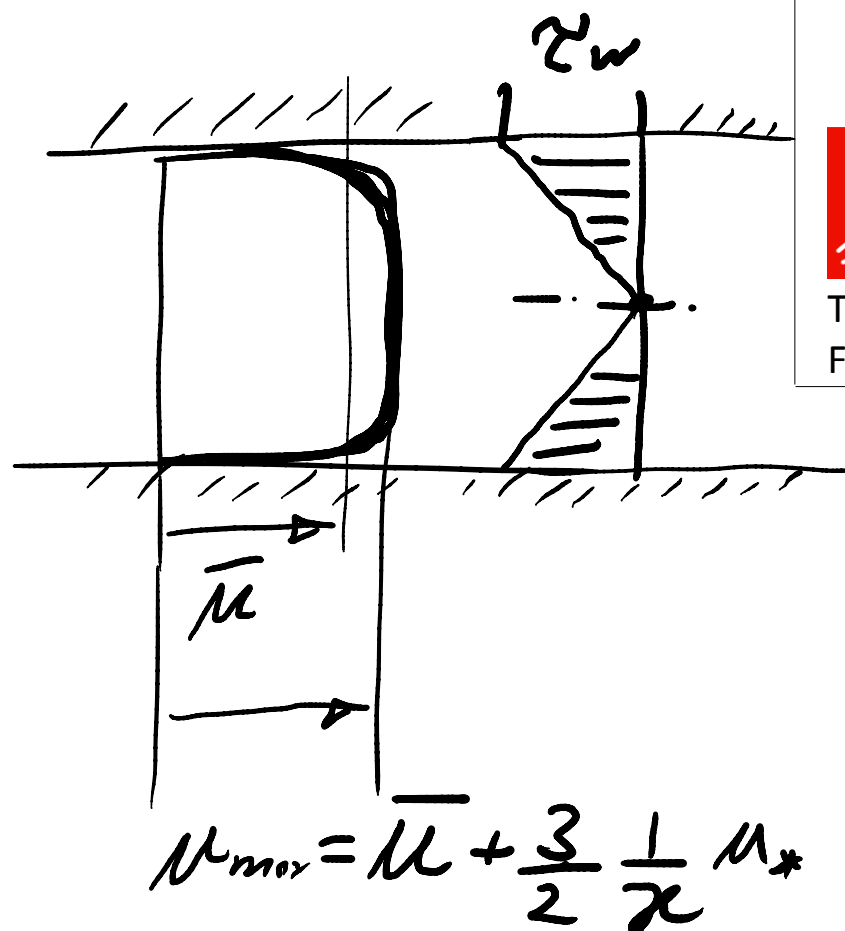


Anm. im Rohr ist

$$u_{max} = 2 \bar{u}$$

Poiseuille-Strömung

od Druckström.



$\kappa = 0.4$ Kármán'sche Konstante

$$u_* = \sqrt{\tau_w / \rho} \text{ Schubspannungsgeschw.}$$